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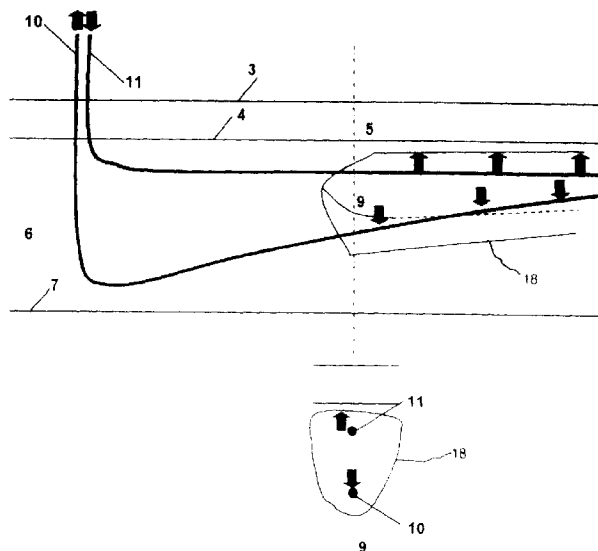
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(54) **Title:** IN SITU HEAVY OIL AND BITUMEN RECOVERY PROCESS



(57) **Abstract:** The present invention is directed to an in situ reservoir recovery process that uses a horizontal well located near the top of a reservoir and an inclined production well to extract bitumen or heavy oil from a reservoir. In a first stage, the top well is used for cold production of reservoir fluids to the surface, in which, reservoir fluids are pumped to the surface in the absence of stimulation by steam or other thermal and/or solvent injection. A lower production well is drilled into the formation below the top well. The top well is converted to an injection well or, if no cold production then a top well is drilled as an injector well. A portion of the bottom well is inclined so that one end of the incline is closer to the injector well than the other end of the incline. In the process, steam circulation creates a heated zone at the point of the two wells that are closest together in the reservoir.

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## ***IN SITU* HEAVY OIL AND BITUMEN RECOVERY PROCESS**

### **TECHNICAL FIELD**

The present invention relates to processes for the recover of heavy oil and bitumen, in particular the use of an inclined portion of a production well within a gravity assisted drainage  
5 process.

### **BACKGROUND**

There are several commercial recovery technologies that are currently used to recover *in situ* heavy oil or bitumen from tar sands reservoirs. In current practice, *in situ*  
10 technologies are used to recover heavy oil or bitumen from deposits that are buried more deeply than about 70 m below which it is no longer economic to obtain hydrocarbon by current surface mining technologies. Most commercial *in situ* processes can recover between about 10 and 60% of the original hydrocarbon in place depending on the operating conditions of the *in situ* process and the geology of the heavy oil or bitumen reservoir. The impact of  
15 variations of oil phase viscosity has been demonstrated by using detailed and advanced reservoir simulation. In addition to permeability, porosity, and oil saturation heterogeneity, oil phase viscosity variations add another complicating and sometimes process dominating feature for producing heavy oil and bitumen reservoirs.

The Steam Assisted Gravity Drainage (SAGD) is described in U.S. Patent No.  
20 4,344,485 (Butler) is used by many operators in heavy oil and bitumen reservoirs. In this method, two horizontal wells, drilled substantially parallel to each other, are positioned in the reservoir to recover hydrocarbons. The top well is the injection well and is located between 5 and 10 meters above the bottom well. The bottom well is the production well and typically located between 1 and 3 meters above the base of the oil reservoir. In the process, steam,  
25 injected through the top well, forms a vapour phase chamber that grows within the oil formation. The injected steam reaches the edges of the depletion chamber and delivers latent heat to the tar sand. The oil phase is heated and as a consequence its viscosity decreases and the oil drains under the action of gravity within and along the edges of the steam chamber towards the production well. In the initial stages of the process, the chamber grows vertically.  
30 After the chamber reaches the top of the reservoir, it grows laterally. The reservoir fluids,

heated oil and condensate, enter the production wellbore and are motivated, either by natural pressure or by pump, to the surface. The thermal efficiency of SAGD is measured by the steam (expressed as cold water equivalent) to oil ratio (SOR), that is CWE m<sup>3</sup> steam / m<sup>3</sup> oil. Typically, a process is considered thermally efficient if its cumulative SOR is between 2 and 3 or lower. There are many published papers and portions of books and regulatory applications that describe the successful design and operation of SAGD. A literature review shows that while SAGD appears to be technically effective at producing heavy oil or bitumen from high quality connected reservoirs, there remains a continued need for well configurations and processes that improve the SOR of SAGD. Currently, the major capital and operating costs of SAGD are tied to the steam generation and water handling, treatment, and recycling facilities.

A variant of SAGD is the Steam and Gas Push (SAGP) process developed by Butler (Thermal Recovery of Oil and Bitumen, Grav-Drain Inc., Calgary, Alberta, 1997}, In SAGP, steam and non-condensable gas are co-injected into the reservoir, and the non-condensable gas forms an insulating layer at the top of the steam chamber. This lowers the heat losses to the cap-rock and improves the thermal efficiency of the recovery process. The well configuration is the same as the standard SAGD configuration.

Examples of literature on design and operation of SAGD in the field include: Butler (Thermal Recovery of Oil and Bitumen, Grav-Drain Inc., Calgary, Alberta, 1997), Komery et al. (Paper 1998.214, Seventh UNITAR International Conference, Beijing, China, 1998), Saltuklaroglu et al. (Paper 99-25, CSPG and Petroleum Society Joint Convention, Calgary, Canada, 1999), Butler et al. (J. Can. Pet. Tech., 39(1): 18, 2000). Examples of literature describing oil composition and viscosity gradients in heavy and bitumen reservoirs include: Larter et al. (2006), Head et al. (2003) and Larter et al. (2003).

There are other examples of processes that use steam or solvent with different well configurations to recover heavy oil and bitumen.

The literature contains many examples of *in situ* methods to recover heavy oil or bitumen economically yet there is still a need for more thermally-efficient and cost-effective *in situ* heavy oil or bitumen recovery technologies, especially when considering the vertical and areal variations of viscosity in the reservoir. There is disclosed herein a method to

recover heavy oil or bitumen from a heterogeneous viscosity reservoir in a manner that is more cost-effective and thermally-efficient than existing methods.

#### FURTHER REFERENCES

5 Further references include:

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## SUMMARY

The present invention relates to a heavy oil or bitumen recovery method. It utilizes an inclined portion within the production well to extend the vapour chamber formation from the injector well. In combination with gravity assisted vapour stimulation processes, the well configuration is designed to enhance the production of heavy oil or bitumen from reservoirs. In one embodiment of the invention, only a portion of the production well is inclined in comparison to the injector well (as examples, H-Well or M-Well and Gravity Assisted Steam Stimulations or "HAGASS" or "MAGASS"). In another embodiment, the production well, inclined along its length (J-Well and Gravity Assisted Steam Stimulation or "JAGASS"), is placed below the injector well whereby the toe of the production well is closest to the injector toe, and the heel of the production well is positioned at a greater distance from the heel of the injector well. The method is applicable to any reservoir, but is especially beneficial in heavy oil and tar sand reservoirs.

The invention also relates to an improved process to recover heavy hydrocarbons from an underground reservoir which shows a vertical or lateral oil mobility gradient controlled by variations in oil viscosity. The method takes advantage of the common vertical changes in oil viscosity in heavy oil tar sand (HOTS) reservoirs and provides a route to initiate earlier production of HOTS petroleum and to ensure maximum vapour chamber growth along the full length of a horizontal vapour injector well.

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## BRIEF DESCRIPTION OF THE DRAWINGS

Embodiments of a heavy oil or bitumen recovery process will now be described by way of example only, with reference to the attached Figures, wherein:

- Fig. 1 is a side and end view of a standard SAGD well configuration;
- Fig. 2 displays a vertical viscosity profile for an Athabasca bitumen reservoir;
- Fig. 3 shows a graph of a vertical viscosity profile for a Peace River tar sand reservoir;

Fig. 4a-l are embodiments of the inclined wells; Fig. 4a-d show side and end cross-sectional views of the JAGASS well configuration and process evolution at four different times respectively; Figures 4e-h show side cross-sectional views of the HAGASS well

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configuration where the production well is inclined at the toe end only; Figure 4i shows the same embodiment as Figures 4e-h but with wells aligned in a linear arrangement; Figures 4j-l are side cross-sectional views of the MAGASS well configuration with an inclined portion in the middle of the production well. In this embodiment a pump would be necessary to produce fluids from the toe of the well;

Fig. 5 is a graph of the performance of standard SAGD and the JAGASS processes as measured by the cumulative oil recovery as a function of time;

Fig. 6a-d show the cumulative steam to oil ratio (cSOR) and thermal efficiencies of the JAGASS embodiment and SAGD; Fig. 6a is a graph that compares the cSOR of standard SAGD and JAGASS processes as a function of time; Figures 6b-d compares the cSOR and thermal efficiency of the JAGASS well configuration to SAGD along the length of the wells; and

Fig. 7 shows injection of steam from a coiled tubing injector.

## 15 DETAILED DESCRIPTION

With reference to the Figures, an inclined well and gravity assisted vapour stimulation process for recovery of *in situ* heavy oil or bitumen from reservoirs is described. The improved process and well configuration will be described with reference to SAGD recovery process. However, a person skilled in the art will understand that other gravity assisted stimulation processes can be used, including steam and solvent recovery processes.

To sustain mobile oil flow to the bottom of the steam chamber under the action of gravity, it is required to create and grow the vapour chamber in an oil reservoir. This produces the density difference between vapour and liquid phases which causes gravity-induced flow of liquid to the production well. The liquid is then removed from the chamber by the production well which delivers it to the surface. To continuously produce oil from the reservoir, the chamber must expand as the process evolves.

It should be noted that the cumulative volume of steam is expressed in terms of the volume of cold water required to produce the steam volume. The following description refers to the attached Figures.

In standard SAGD, as shown in Figure 1, a horizontal production well 1 is drilled into the oil reservoir 6 penetrating the surface of the earth 2 and overburden materials 5. The reservoir is bounded on the top and bottom by the surface 4, the bottom of the overburden, and by the surface 7, the top of the understrata. Above the oil reservoir is the overburden 5, which is of any one or more of shale, rock, sand layers, and aquifers. A horizontal injection well 2, typically aligned vertically between five and ten meters above the production well 1 is also drilled into the reservoir 6. In standard SAGD, steam is injected into the reservoir through the injection well 2 and flows into the steam depletion chamber 8. In substantially vapour form, steam flows to the edges of the chamber 8, condenses, and delivers its latent heat to the tar sand 9 within the reservoir unit. As reservoir fluids are produced to the surface with the production well 1, the steam chamber 8 expands further into the oil reservoir. The injected steam acts to deliver both heat and pressure to the reservoir. After the oil in the reservoir 8 is heated, its viscosity falls, it becomes more mobile, and it flows under gravity to the production well 1.

In Figure 2, a typical viscosity profile for an Athabasca bitumen reservoir is displayed. At the top of the oil-bearing formation, the live oil viscosity is roughly equal to 15,000 cP whereas at the bottom is it equal to about 250,000 cP at reservoir temperature. Figure 3 shows a graph of the viscosity of the oil phase in Peace River tar sand with depth. Here, it varies from 10,000 cP at the top to 260,000 centipoise cP at the bottom at reservoir temperature. In Figure 3, the viscosity of Cold Lake heavy oil with depth is plotted. Figures 2 and 3 show that viscosity variations in heavy oil and bitumen reservoirs can have order of magnitude differences between the value at the top and the value at the bottom of the reservoir.

As shown in Figures 4a, 4b, 4c, and 4d, a top horizontal well 11 is drilled into the reservoir 6 penetrating the surface of the earth 3 and the overburden 5. At the top and bottom of the reservoir are the bottom surface of the overburden 4 and top surface of the understrata 7. The horizontal well 11 lies in the reservoir 6, and has a heel and toe. A production well 10 lies in the reservoir 6 below the horizontal well 11 and has a heel and toe, with the toe higher than the heel in the reservoir so that the well is inclined. In some embodiments, the toes of the wells 10, 11 are closer to each other than the heels of the wells 10, 11. In some embodiments,

the well 11 is mainly used as an injection well and is connected to surface injection equipment. In some embodiments, the well 10 is mainly used as a production well and is connected to surface production equipment.

In one embodiment of the process, in a first stage (Stage 1) of the process, displayed in Figure 4a, reservoir fluids are produced from the reservoir as is done in cold production of heavy oil and bitumen. In this stage of the process, no injectants are introduced into the reservoir. In this stage of production, between 1 and 20 volume % of the original hydrocarbon in place in the reservoir is produced depending on the economic benefit the process yields during its operation. In the second stage of the process (Stage 2), displayed in Figures 4b, 4c, and 4d, a second inclined well 10 is drilled into the oil formation in vertical alignment with the top horizontal well 11. Then, an injectant, acting as a hydrocarbon mobilizer, is injected into the oil reservoir through the top well 11 and reservoir fluids are produced through the bottom inclined well 10.

The injectant may be any suitable fluid that mobilizes hydrocarbons in the reservoir. In various embodiments, for example, the injectant may be water, steam, carbon dioxide, air, nitrogen or hydrocarbon solvent in the liquid or vapour phase. Suitable hydrocarbon solvents include C<sub>1</sub>-C<sub>10</sub> alkanes, aromatics and alcohols. Combinations of these injectants may be used. In the case of air or a gas comprising, in some portion, oxygen being added as an injectant, a controlled burn of hydrocarbons created by igniting a flame front within the reservoir maybe be used to mobilize hydrocarbons. The injectant may operate by displacing reservoir hydrocarbons in a displacement mechanism, or by reducing the viscosity of the reservoir hydrocarbons so that they move by operation of gravity towards the production well 10. Viscosity reduction may be caused by heating, or by dissolution of the injectant in the reservoir hydrocarbons, or by solvent-induced precipitation or phase separation of the heavier components of the reservoir hydrocarbons leading to a more mobile lighter oil phase. Combinations of these mobilizing methods may be used, as for example using a heated solvent, with or without added displacement gas.

Prior to the start of production, it is desirable to establish a communication path between the top well 11 and the bottom well 10. This may be initially established by injection of injectant into either or both the top well 11 and bottom well 10, and should start at the toe,

as illustrated in Fig. 4b. When steam is used as the injectant, a steam circulation interval may be used to establish thermal communication between the top and bottom wells. The steam provides a means to deliver energy and pressure to the reservoir. Steam circulation interval is the practice of passing hot steam through one or both of the injection and production wells to heat the formation materials immediately adjacent and surrounding the wells to sufficient temperature that the oil phase in this region has reduced viscosity and improved mobility. For example, the steam passes into the wells through a tubing string and is produced to the surface via the annular space between the tubing string and the well liner and casing. Typically, little steam is injected into the reservoir although some reservoir fluids may be produced due to thermal expansion of the reservoir fluids on heating.

Injection of injectant into one or both of the wells 10, 11, creates a vapour and mobilized hydrocarbon chamber 19, which in one embodiment will start at the toes of the wells 10, 11. Injectant injected into the oil reservoir from well 11 flows to the edges of the chamber 19. In the case of steam used as an injectant, the steam condenses and releases its latent heat to the oil sand heating it and consequently lowering the oil phase viscosity enabling it to flow under the action of gravity to the production well 10. As the process evolves and oil is produced to the surface, as shown in Figures 4b, 4c, and 4d, the mobilized hydrocarbon chamber 19 expands into the reservoir 5 and along the wells 10 and 11 in the upwell direction.

As an alternate embodiment of the process, the process can be started from the second Stage alone, that is, without the cold production Stage. In this case, referring to Figure 4b, the process will operate starting with the establishment of fluid communication between the top injection well 11 and bottom inclined production well 10. After communication is established, injectant is injected through the top well 11 into the chamber 19 and reservoir fluids are produced from the bottom well 10. Then the production process continues as shown in Figures 4c and Figure 4d.

After production is initiated, it can be maintained in some embodiments by continuing to inject injectant in a manner such that the mobilized hydrocarbon chamber 18 moves upwell. For example, in the case of steam, this may be accomplished using a modified SAGD procedure with a steam trap pressure control to prevent steam breakthrough or by

injecting steam in the injector from a coiled tubing steam injector insert shown in Fig. 7 which allows the steam entry point to migrate back along the well bore during production as the chamber 19 develops. A similar technique, in which injectant is injected into the top well as a coiled tubing system is withdrawn from the well 11, may be used for continued production using other injectants.

5 Steam trap control refers to the practice of controlling the production rate or production well pressure so that there is a liquid bath surrounding the production well. This prevents steam from passing directly from the injection well to the production well. Figure 7 shows an embodiment of continued injectant injection using coiled tubing X1. The coiled tubing X1 is inserted into the injection well with an injector insert X2 that has been partially withdrawn and lies approximately at the middle of the injection well 11. The insert can be as simple as the open end of the coiled tubing or may involve packers, valves or other devices to control flow. Sensors may be introduced to one or both the wells to detect the boundaries of the mobilized hydrocarbon chamber 18, and thus determine where and how much injectant to inject. In the case of use of steam as the injectant, steam breakthrough can be monitored using H and O stable isotopic signatures of water to facilitate real-time detailed control as well as from temperatures measured in the production well measured from thermocouples X3 placed along the production well. In an alternative embodiment, if the gas is used as an injectant, some gas, as for example steam, can be allowed to be produced into the production wellbore to have lift to promote reservoir fluids to be produced to the surface. One benefit is that the interwell communication would most likely occur at the toe (location of minimum interwell distance) which means that injectant will flow the length of the production well, increasing hydrocarbon mobility in and around the production well, and increasing production pressure. In the case of use of a heated injectant, the injectant will help to keep the production well at elevated temperature to enhance flow of the more viscous oils located in the lower parts of the reservoir along the wellbore.

Figures 4b-d show a J-shaped production well with an incline along the entire length of the well. However, the production well does not need to be inclined along its entire length. For example, Figures 4e-h show a production well with an inclined section at the toe end (HAGASS). As shown, the vapour chamber forms at the toe of the wells and starts gravity

drainage. The creation of the vapour chamber follows the incline and towards the heel of the well. As shown in Figure 4i, a linear pattern of injection and production wells takes advantage of the vapour chamber formation and thermal efficiencies to increase production. Further, one injector well can be used for more than one production well to reduce the capital expenditures in oil recovery. Figures 4j-1 show a further embodiment where the inclined portion occurs in the middle of the production well (MAGASS). In such a configuration, two production wells would be required.

Computer-aided reservoir simulation can be used to predict pressure, oil, solvent, water, and gas production rates, and vapour chamber dimensions to help design the well placement and operating strategy. Also, the reservoir simulation calculations can be used to assist in the estimation of the time intervals of Stage 1 depicted in Figure 4a (cold production) and Stage 2 displayed in Figures 4b to 4d (mobilized hydrocarbon drainage by using an inclined production well). Prior to executing the process in the field, a reservoir simulation study of the recovery process would be done to help plan the well configuration and operating strategy.

Figure 5 compares the cumulative production of oil from field scale numerical model predictions in an Athabasca reservoir with vertical viscosity variations according to Figure 2 between the standard SAGD and thermal JAGASS process (process where only Stage 2 as described above is done). The results reveal that the JAGASS process produces substantially more oil than the standard SAGD process.

Figure 6a displays the cumulative steam to oil ratio (cSOR) from field scale numerical model predictions of the standard SAGD and JAGASS processes. The cSOR is a measure of the thermal efficiency of the process and is closely correlated with the economic performance of the recovery processes. The results show that the JAGASS process is thermally more efficient than the standard SAGD process. Figures 6b-d show the cSOR and thermal efficiency of the JAGASS process along the length of the wells as compared to SAGD. These graphs show that the cSOR and thermal efficiency at the toes of the injector and production wells are the same for the J-well configuration as for SAGD. However, moving along the incline of the production well, as the distance between the wells increases, the cSOR and the thermal efficiency for the J-well is greater than that for SAGD.

In an alternative embodiment of the process, the injectant pressure and temperature can be changed throughout the operation of the process to improve the thermal efficiency of the process. For example, in the early stages of the process before the mobilized hydrocarbon chamber 18 has reached the top of the oil-rich interval, the injection pressure and corresponding saturation temperature could be high thus providing relatively high rates of oil production. Later, after the mobilized hydrocarbon chamber 19 has reached the top of the oil zone, the operating pressure and corresponding saturation temperature can be reduced so that heat losses to the overlying cap rock is reduced. This improves the overall thermal efficiency of the process. The pressure and temperature of the process can be measured by pressure sensors and thermocouples or other devices located in the injection or production wells or both as well as observation wells. Also, the pressure of the mobilized hydrocarbon chamber 18 can be estimated from the injection pressure at the injection well head by taking pressure losses in the well into account. A reduction of the pressure in the chamber can be obtained by reducing the amount of injectant injected into the oil reservoir or by raising the production rate of fluids from the reservoir. An alternative method to lower the injectant partial pressure and corresponding injectant saturation temperature can be accomplished by adding an additive to the injected steam.

In an embodiment of the process, a steam additive can be added to injected steam to enhance the production rates of oil. A solvent, whether used in combination with other injectants or on its own, can lower the viscosity of the oil phase thus raising its mobility and therefore its production rate. A non-condensable gas additive for steam injection can also replace a fraction of the volume of steam injected into the reservoir thus raising the thermal efficiency of the process. Examples of solvent additives include the C<sub>2</sub> to C<sub>10</sub> hydrocarbons such as propane, hexane, or a mixture as would be the case with diluent or gas condensates. Examples of gases include methane, carbon dioxide, nitrogen, or air.

In an additional embodiment of the process, at the end of the process, a blowdown stage can be started in which no injectant is injected into the oil formation and the pressure of the mobilized hydrocarbon chamber is lowered while fluids are continuously produced to the

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surface. In this stage, because no injectant is being injected, the process is thermally very efficient (oil production with no injection). However, the oil rate declines rapidly because no additional heat is being injected into the reservoir and heat losses to the understrata and overburden start to consume the remaining heat in the oil zone.

5           In another embodiment of the present invention, the present process can be used to enhance recovery of heavy oil and bitumen from reservoirs that have vertical and/or areal viscosity gradients.

          Compositional and fluid property gradients are common and documented in conventional heavy oilfields and in super heavy oil occurrences such as tar sand reservoirs. In  
10 the severely biodegraded oils of the Western Canadian tar sand reservoirs, highly non-linear chemical compositional and fluid viscosity gradients are common in both Athabasca and Peace River reservoirs (Larter et al., 2006). The variations in dead oil viscosity can be determined by mechanical recovery of the oil or bitumen with a centrifuge followed by measurements using a viscometer, or by solvent extraction and use of molecular composition  
15 and viscosity correlations. The molecular level variations in compositions are proxies for overall bitumen composition and thus viscosity, the actual compound suites most suitable to assess fluid properties varying with level of degradation and oil type. This is easily determined by using standard geochemical protocols and data analysis procedures that look for compound groups that show reproducible changes in composition over the viscosity range  
20 of application interest. Comparison of oil or bitumen molecular fingerprints from solvent extracted bitumens in reservoir core or cuttings, with similar sets of analyses on calibration sets of spun or otherwise extracted raw bitumen, allows for estimation of dead oil viscosities solely from the geochemical measurements and allow viscosity profiling of reservoirs to be carried out at meter scale resolution (Larter et al., 2006). These high resolution viscosity logs  
25 are essential for optimizing well locations in JAGASS and other thermal recovery processes using intelligent cold and thermal recovery techniques. This geochemical fluid property prediction approach allows for production of routine and rapid high resolution viscosity logs from core or cuttings or analysis of cuttings from horizontal wells. As heavy oil compositions commonly vary along well sections, the oil heterogeneity assessed from either core or  
30 cuttings, if appropriate samples are taken and stored, can also be used to allocate production

to reservoir zones by using produced oil and multivariate deconvolution data analysis techniques. This is especially useful in allocation of production in horizontal wells and can be used to assess the effectiveness of the recovery well locations and to optimize well operations including steam and other injected fluid cycling sequences.

5           Dead oil viscosities are converted to live oil viscosities using gas solubility estimates as a function of reservoir pressure data and correlations between gas to oil ratio, live and dead oil viscosity. The dependence of oil viscosity on recovery temperature is determined by using measurements of viscosity on the same oil samples at various temperatures relevant to the recovery process. Thus, a profile through the oil column of viscosity as a function of  
10 temperature is obtained.

          At *in situ* initial conditions i.e. temperature and pressure, heavy oil and bitumen have much higher viscosity than conventional light oils. Also, the defining characteristic of heavy and super heavy oilfields is the large spatial variation in fluid properties, such as oil viscosity, commonly seen within the reservoirs. Heavy oil and tar sands are formed by microbial  
15 degradation of conventional crude oils over geological timescales. Large-scale lateral and small-scale vertical variations in fluid properties due to interaction of biodegradation and charge mixing are common, with up to orders of magnitude variation in in-reservoir viscosity over the thickness of a reservoir. Constraints such as oil charge mixing, reservoir temperature-dependant biodegradation rate and aqueous nutrient supply to the organisms ultimately dictate  
20 the final distribution of viscosity found in heavy oil fields. Head et al. (2003); Larter et al. (2003; 2006); Huang et al. (2004).

          The impact of viscosity variations in a heavy oil reservoir on heavy oil and bitumen productivity depends on the recovery method. Cold heavy oil production with sand (CHOPS) is critically influenced by oil viscosity and published literature (Larter et al., 2006) reveals  
25 that vertical viscosity gradients can substantially impact both existing steam assisted gravity drainage and cyclic steam stimulation operations if the gradients are not built into simulation protocol and well design procedures. (Larter et al., 2006).

          Use of an inclined production well, as set out above, in combination the heavy oil or bitumen recovery method results in increased heavy oil or bitumen production. The inclined  
30 production well, or inclined portion of the production well, extends through the viscosity

gradients within the reservoir. This allows for the earlier production of hydrocarbons and ensures maximum vapour chamber growth along the full length of the horizontal vapour injector well than with traditional methods.

5 The embodiments of the process described above are examples. A person skilled in this art understands that variations and modifications of the process can be done without departing from the scope of the claims. Such variations and modifications fall within the scope of the present invention.

**CLAIMS:**

1. A method to recover heavy hydrocarbons from an underground reservoir, the method comprising the steps of:
- 5 a) providing a well located near the top of the reservoir in the oil formation where the oil phase viscosity at the top is relatively low and producing reservoir hydrocarbons from this well under cold production conditions (non-thermal);
- b) at a later time, drilling a lower inclined well that has its toe relatively close to the toe of the top well and heel deeper in the oil formation below the heel of  
10 the top well,
- c) injecting injectant into the top well and producing reservoir fluids from the lower production well; and
- d) continuing to inject injectant into the top well and producing reservoir fluids while growing a vapour and mobilized hydrocarbon chamber in the upwell (toe  
15 to heel) direction along the wellpair.
2. The method of claim 1 further comprising the step of circulating steam through the injection and production wells to establish thermal communication between the two wells.
- 20 3. The method of claim 1 further comprising the step of monitoring and changing injection pressure to adjust the operating temperature of the process in steps a) through d).
4. The method of claim 1 further comprising the step of using combinations of injectants in steps a) through d).
- 25 5. The method of claim 1 whereby a blowdown period where injection ceases and the pressure is reduced at the end of the economic life of the process to recover heavy oil or bitumen from the reservoir.

6. The method of claim 1 whereby the phase behaviour of the injectant is controlled by monitoring well pressures and temperatures.
7. The method of claim 6 wherein the injectant is steam and phase behaviour of the injectant is controlled to maintain steam trap control such that liquid water covers the production well while a steam chamber surrounds the injection well.
8. The method of claim 6 wherein the injectant is air and the reaction behaviour of the injectant with a small fraction of the reservoir hydrocarbons is controlled to obtain mobilized hydrocarbons.
9. The method of claim 8 wherein the reaction behaviour of the injectant with hydrocarbons in the reservoir comprises igniting a controlled hydrocarbon flame front within the reservoir.
10. The method of claim 1 wherein injectant is injected into the top well through coiled tubing that is pulled back through the top well.
11. The method of claim 10 wherein the coiled tubing is pulled back to follow the produced oil front.
12. The method of claim 10 wherein in-well control valves are used to control steam delivery in the top well.
13. A method to recover heavy hydrocarbons from an underground reservoir, the method comprising the steps of:
- a) providing a well located near the top of the reservoir in the oil formation where the oil phase viscosity at the top is relatively low;
  - b) drilling a lower inclined well that has its toe relatively close to the toe of the top well and heel deeper in the oil formation below the heel of the top well,

- c) injecting injectant into the top well and producing reservoir fluids from the lower production well; and
- d) continuing to inject injectant into the top well and producing reservoir fluids while growing a vapour and mobilized hydrocarbon chamber in the upwell (toe to heel) direction along the well pair.

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14. The method of claim 13 further comprising the step of circulating steam through the injection and production wells to establish thermal communication between the two wells.

10 15. The method of claim 13 further comprising the step of monitoring and changing injection pressure to adjust the operating temperature of the process in steps a) through d).

16. The method of claim 13 further comprising the step of using combinations of injectants in steps a) through d).

15

17. The method of claim 13 whereby a blowdown period where injection ceases and the pressure is reduced at the end of the economic life of the process to recover heavy oil or bitumen from the reservoir.

20 18. The method of claim 13 whereby the phase behaviour of the injectant is controlled by monitoring well pressures and temperatures.

19. The method of claim 18 wherein the injectant is steam and phase behaviour of the injectant is controlled to maintain steam trap control such that liquid water covers the production well while a steam chamber surrounds the injection well.

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20. The method of claim 18 wherein the injectant is air and the reaction behaviour of the injectant with a small fraction of the reservoir hydrocarbons is controlled to obtain mobilized hydrocarbons.

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21. The method of claim 20 wherein the reaction behaviour of the injectant with hydrocarbons in the reservoir comprises igniting a controlled hydrocarbon flame front within the reservoir.

5 22. The method of claim 13 wherein injectant is injected into the top well through coiled tubing that is pulled back through the top well.

23. The method of claim 22 wherein the coiled tubing is pulled back to follow the produced oil front.

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24. The method of claim 22 wherein in-well control valves are used to control steam delivery in the top well.

15 25. A method to recover heavy hydrocarbons from an underground reservoir, wherein the underground reservoir has a top well located near the top of the reservoir in the oil-bearing formation, the method comprising the steps of:

- 20 a) providing a lower production well with an inclined portion having one end of the inclined portion relatively close to the top well and the other end of the inclined portion being deeper in the oil formation,
- b) injecting injectant into the top well and producing reservoir fluids from the lower production well; and
- c) continuing to inject injectant into the top well and producing reservoir fluids while growing a vapour and mobilized hydrocarbon chamber in the upwell direction along the well pair.

25

26. The method of claim 25 further comprising the step of circulating steam through the top and lower wells to establish thermal communication between the two wells.

30 27. The method of claim 25 further comprising the step of monitoring and changing injection pressure to adjust the operating temperature of the process in steps a) through c).

28. The method of claim 25 further comprising the step of using combinations of injectants in steps a) through c).
- 5 29. The method of claim 25 where a blowdown period where injection ceases and the pressure is reduced at the end of the economic life of the process in order to recover heavy oil or bitumen from the reservoir.
- 10 30. The method of claim 25 whereby the phase behaviour of the injectant is controlled by monitoring well pressures and temperatures.
- 15 31. The method of claim 30 wherein the injectant is steam and phase behaviour of the injectant is controlled to maintain steam trap control such that liquid water covers the production well while a steam chamber surrounds the injection well.
- 20 32. The method of claim 30 wherein the injectant is air and the reaction behaviour of the injectant with a small fraction of the reservoir hydrocarbons is controlled to obtain mobilized hydrocarbons.
- 25 33. The method of claim 32 wherein the reaction behaviour of the injectant with hydrocarbons in the reservoir comprises igniting a controlled hydrocarbon flame front within the reservoir.
34. The method of claim 25 wherein the injectant is injected into the top well through coiled tubing that is pulled back through the top well.
35. The method of claim 34 in which the coiled tubing is pulled back to follow the produced oil front.

36. The method of claim 34 in which in-well control valves are used to control steam delivery in the top well.

37. A method to recover heavy hydrocarbons from an underground reservoir, wherein the underground reservoir has a top well located near the top of the reservoir in the oil formation, the method comprising the steps of:

- a) providing a lower inclined well with a toe relatively close to the toe of the top well and a heel deeper in the oil formation below the heel of the top well,
- b) injecting injectant into the top well and producing reservoir fluids from the lower production well; and
- c) continuing to inject injectant into the top well and producing reservoir fluids while growing a vapour and mobilized hydrocarbon chamber in the upwell direction along the well pair.

38. The method of claim 37 further comprising the step of circulating steam through the top and lower wells to establish thermal communication between the two wells.

39. The method of claim 37 further comprising the step of monitoring and changing injection pressure to adjust the operating temperature of the process in steps a) through c).

40. The method of claim 37 further comprising the step of using combinations of injectants in steps a) through c).

41. The method of claim 37 where a blowdown period where injection ceases and the pressure is reduced at the end of the economic life of the process in order to recover heavy oil or bitumen from the reservoir.

42. The method of claim 37 whereby the phase behaviour of the injectant is controlled by monitoring well pressures and temperatures.

43. The method of claim 42 wherein the injectant is steam and phase behaviour of the injectant is controlled to maintain steam trap control such that liquid water covers the production well while a steam chamber surrounds the injection well.

5 44. The method of claim 42 wherein the injectant is air and the reaction behaviour of the injectant with a small fraction of the reservoir hydrocarbons is controlled to obtain mobilized hydrocarbons.

10 45. The method of claim 44 wherein the reaction behaviour of the injectant with hydrocarbons in the reservoir comprises igniting a controlled hydrocarbon flame front within the reservoir.

46. The method of claim 37 wherein the injectant is injected into the top well through coiled tubing that is pulled back through the top well.

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47. The method of claim 46 in which the coiled tubing is pulled back to follow the produced oil front.

20 48. The method of claim 46 in which in-well control valves are used to control steam delivery in the top well.

49. Apparatus for production of hydrocarbons from a reservoir, the apparatus comprising:

an injector horizontal well lying in the reservoir;

25

a production horizontal well lying in the reservoir below the injector well;

the second horizontal well having an inclined portion, the inclined portion having a top end and a lower end;

the top end of the inclined portion being closer to the injector well than the lower end of the inclined portion; wherein the production well is useful in gravity drainage

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production processes.

50. The apparatus of claim 49 wherein the production well has a J-shape.

51. The apparatus of claim 49 in which the first horizontal well is connected to injection equipment and the second horizontal well is connected to production equipment.

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52. Apparatus for production of hydrocarbons from a reservoir, the apparatus comprising:

a first horizontal well lying in the reservoir, and having a first heel and a first toe;

a second horizontal well lying in the reservoir below the first horizontal well, the

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second horizontal well having a second heel and a second toe; and

the second toe being higher in the reservoir than the second heel.

53. The apparatus of claim 52 wherein the first toe is closer to the second toe than the first heel is to the second heel.

15

54. The apparatus of claim 52 in which the first horizontal well is connected to injection equipment and the second horizontal well is connected to production equipment.

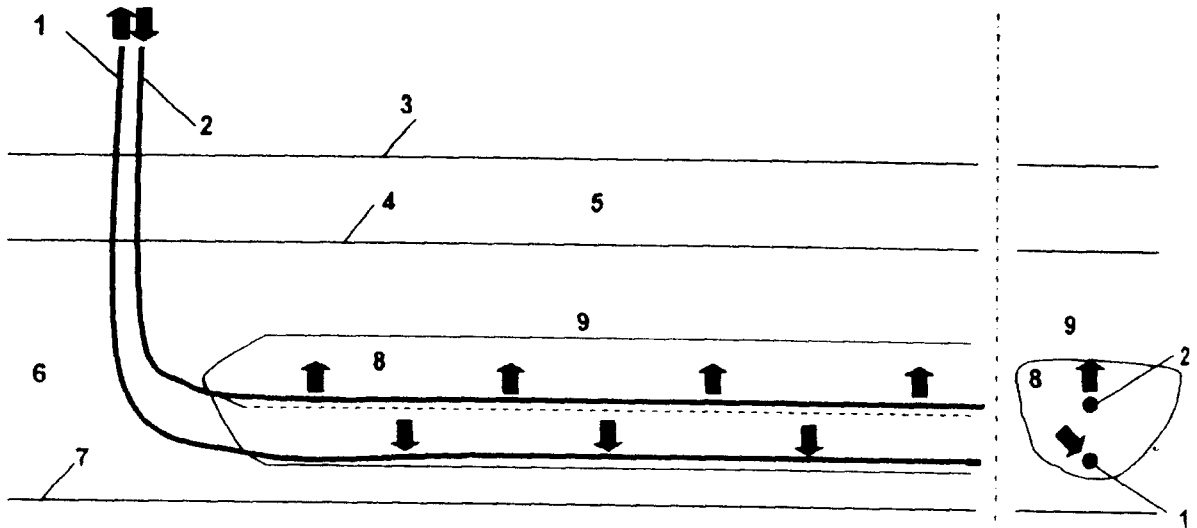


Figure 1

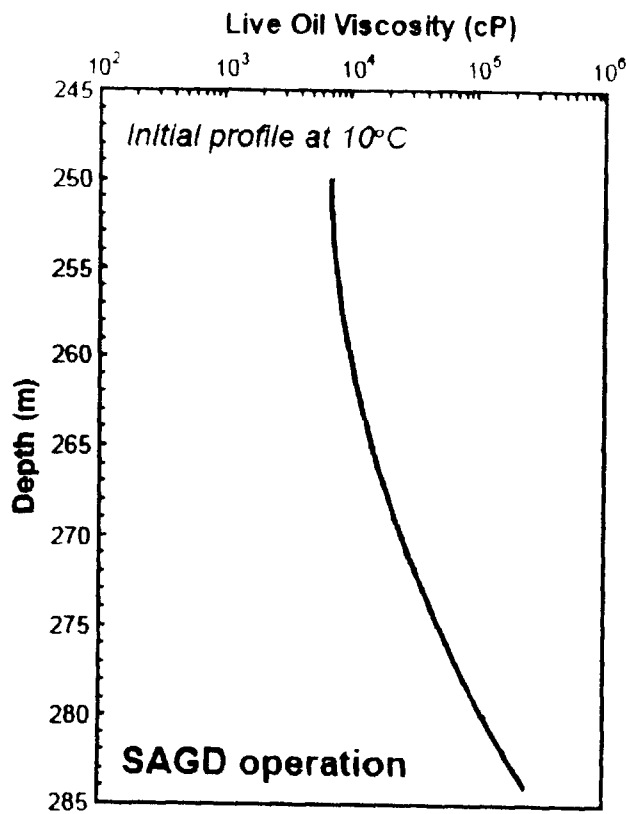


Figure 2

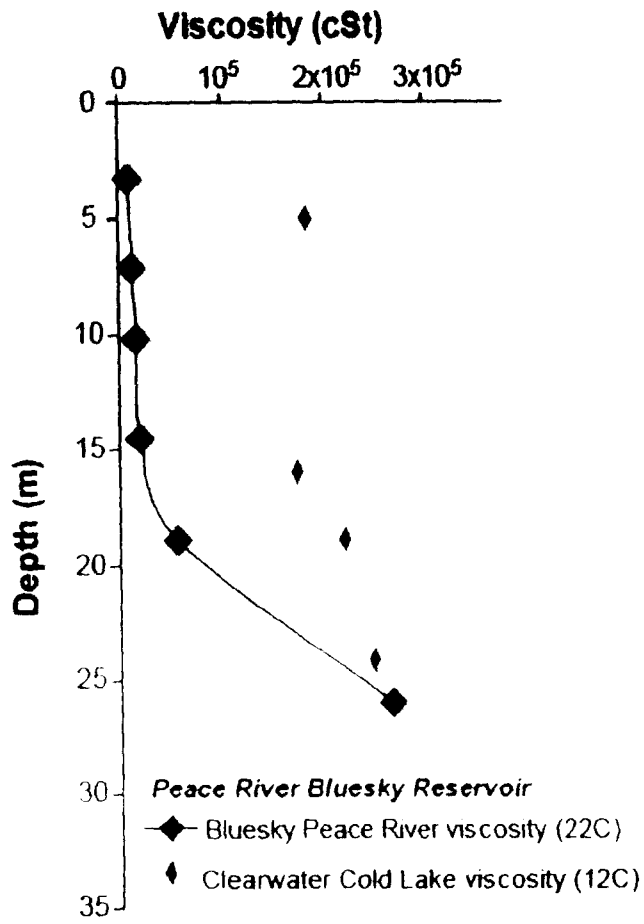


Figure 3

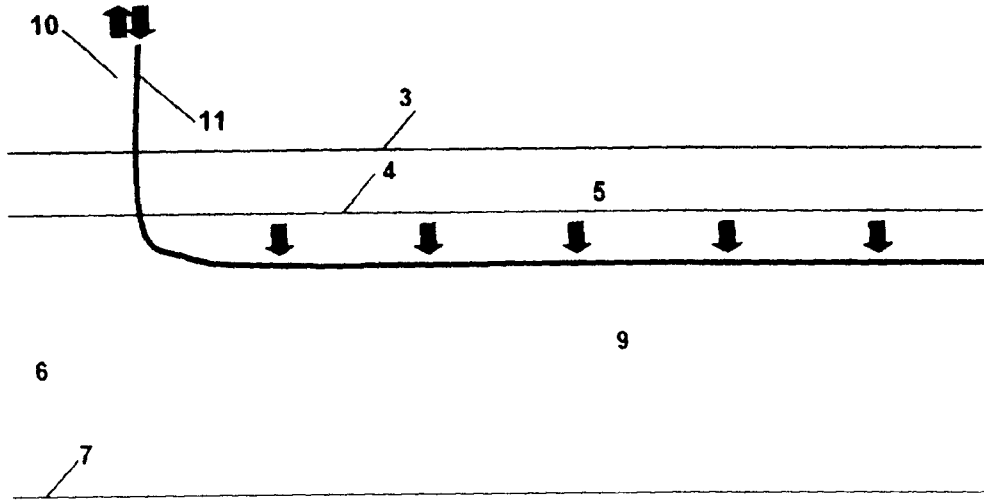


Figure 4a

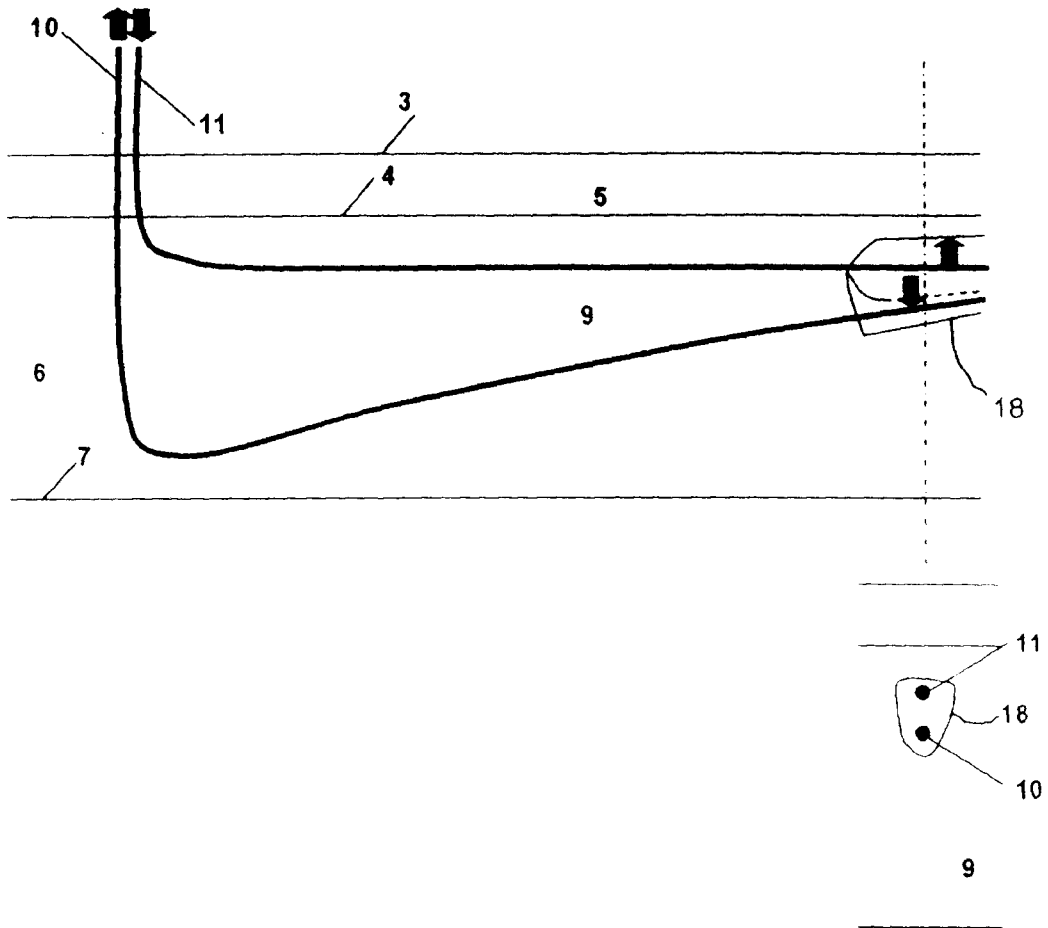


Figure 4b

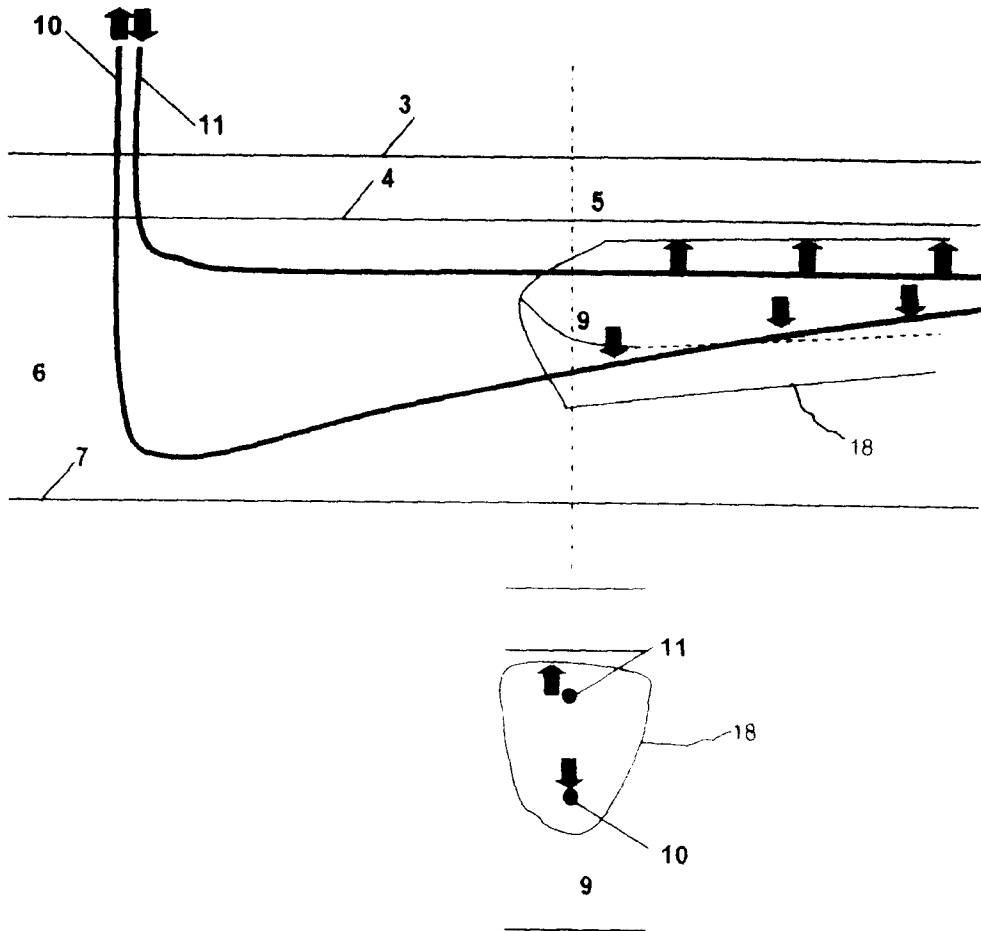


Figure 4c

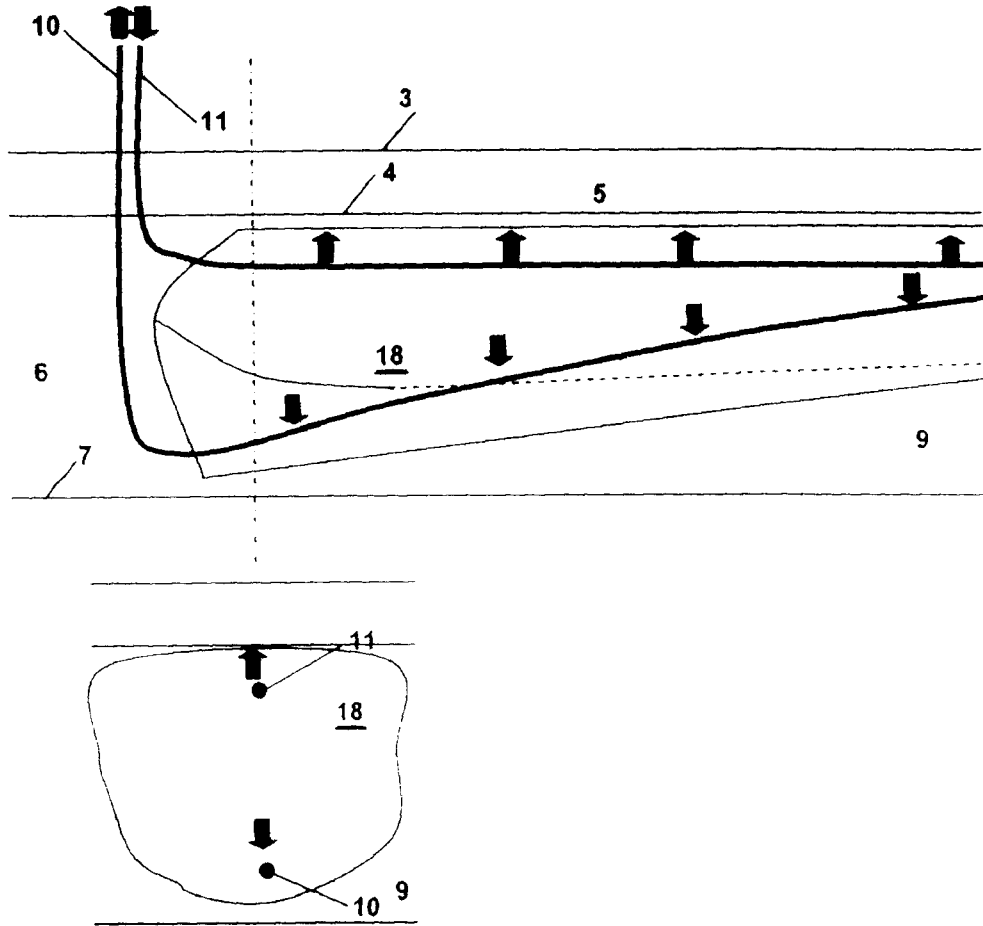


Figure 4d

# HAGASS: Phase 2

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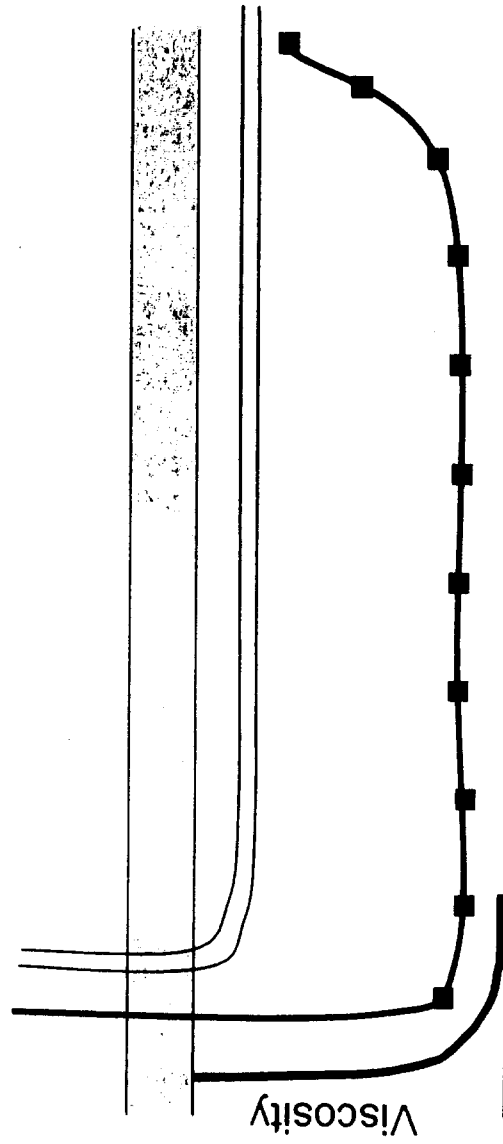


Figure 4e

# HAGASS: Phase 2

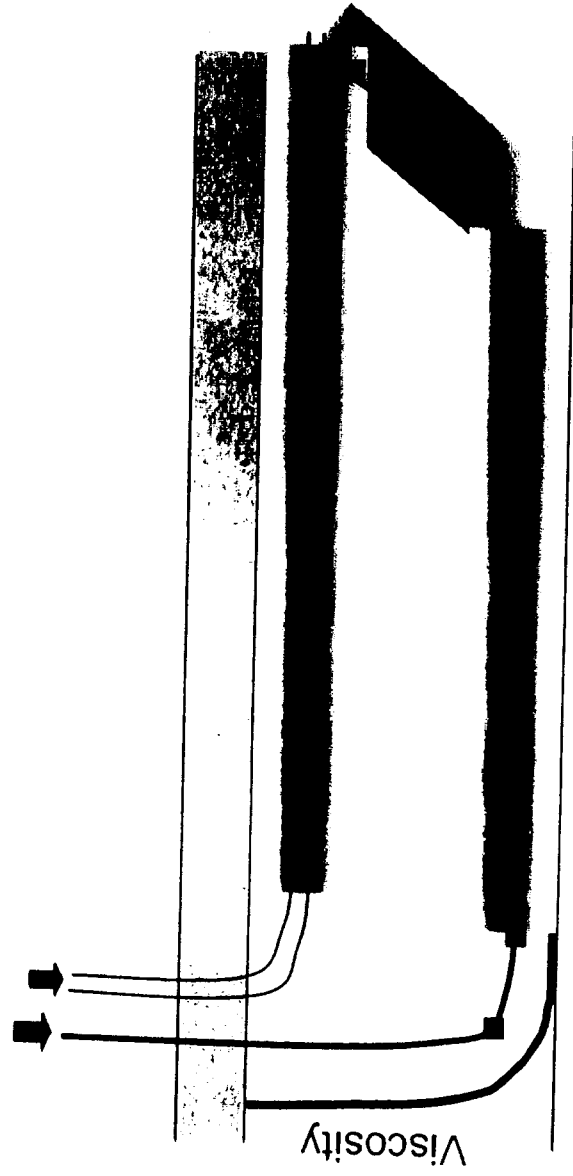


Figure 4f

# HAGASS: Phase 2

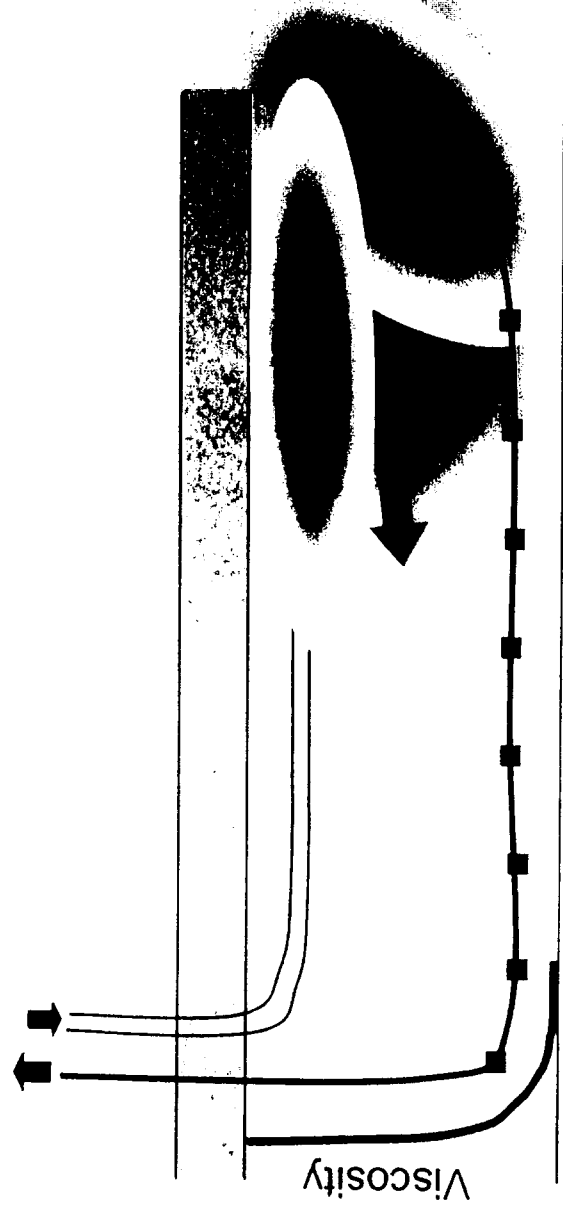


Figure 4g

# HAGASS: Phase 2

10/20

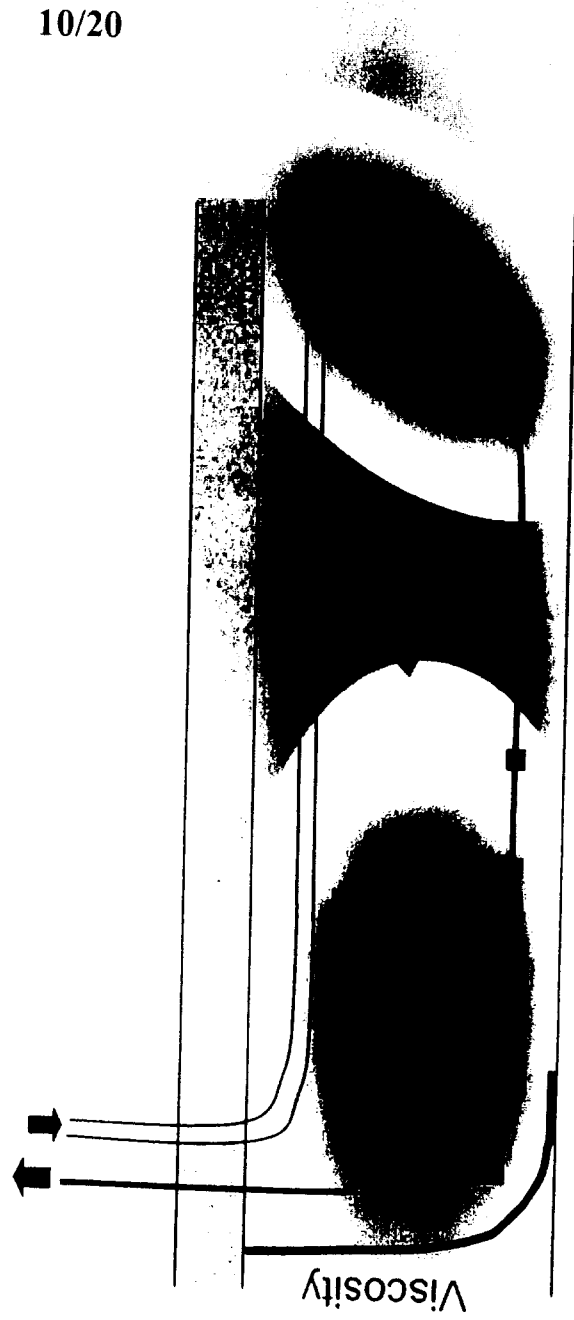


Figure 4h

# HAGASS: Phase 2

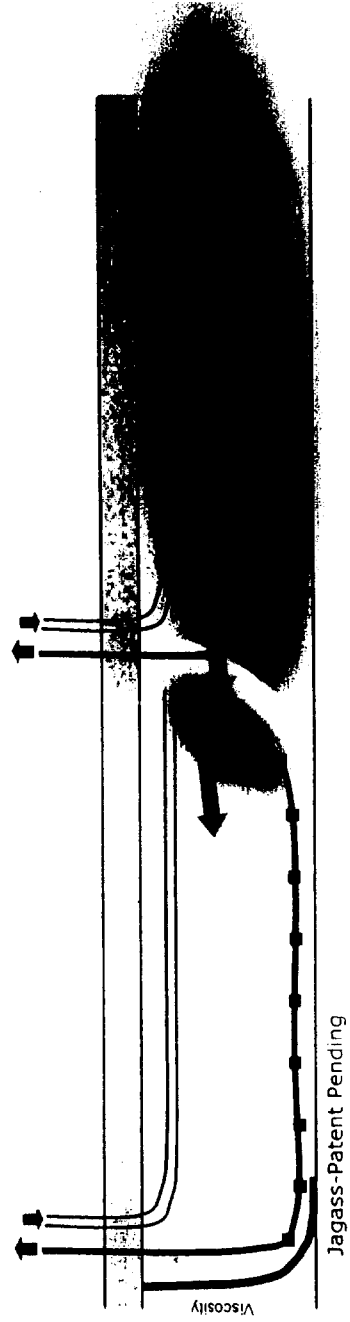


Figure 4i

# MAGASS: Phase 2

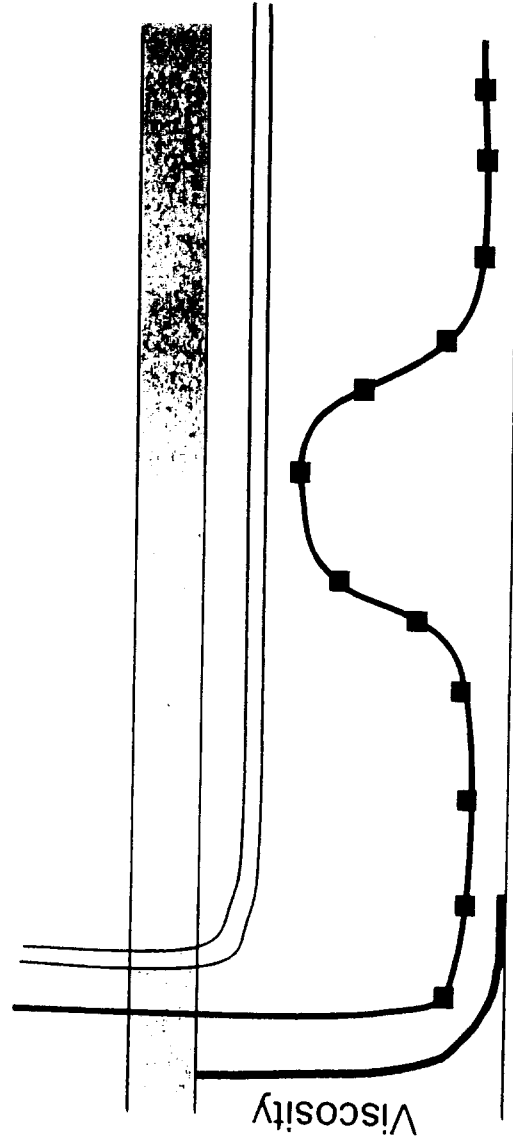


Figure 4j

# MAGASS: Phase 2

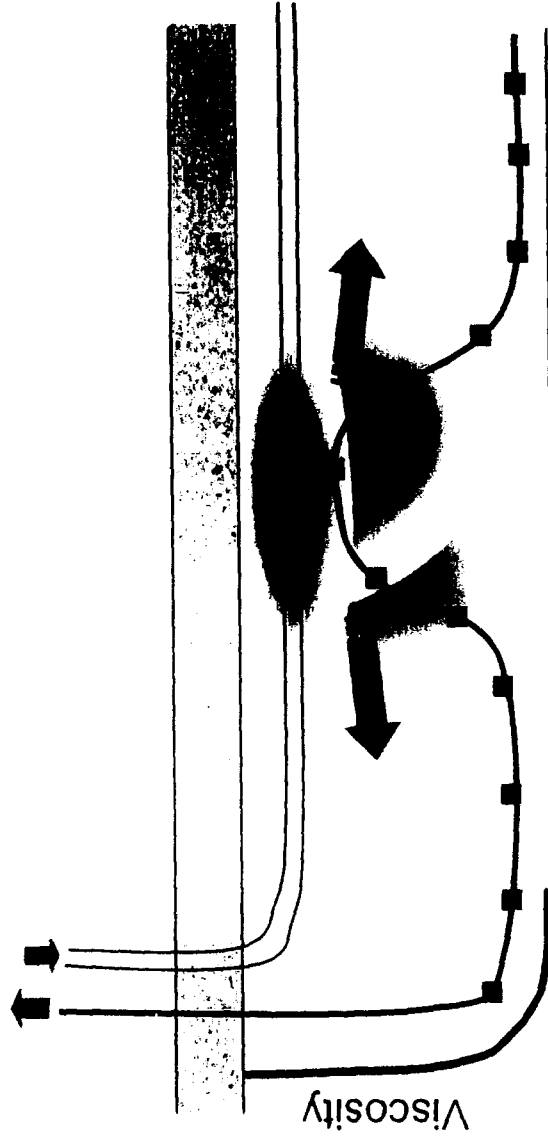


Figure 4k

# HAGASS: Phase 2

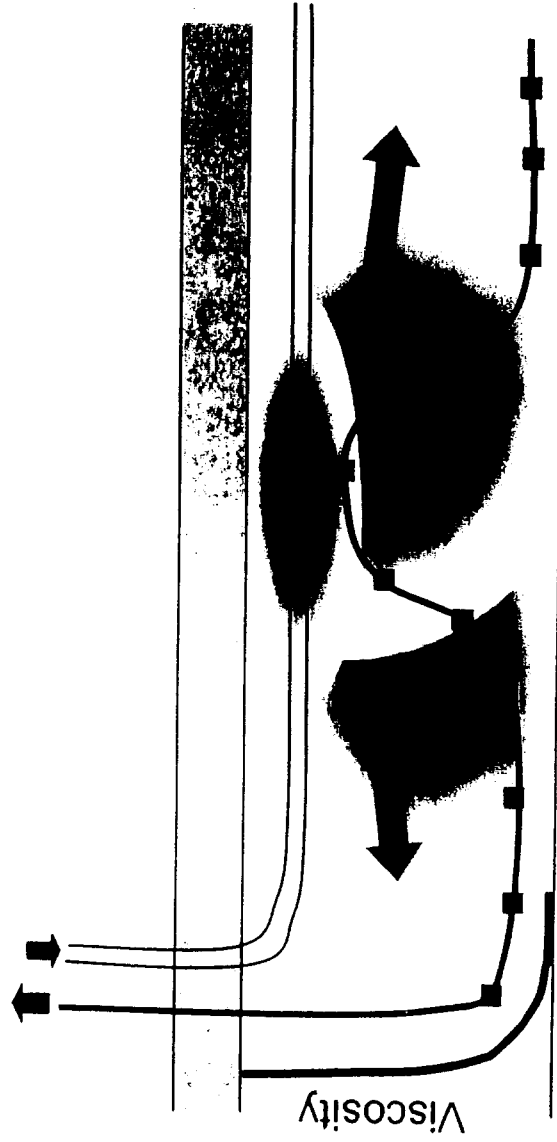


Figure 41

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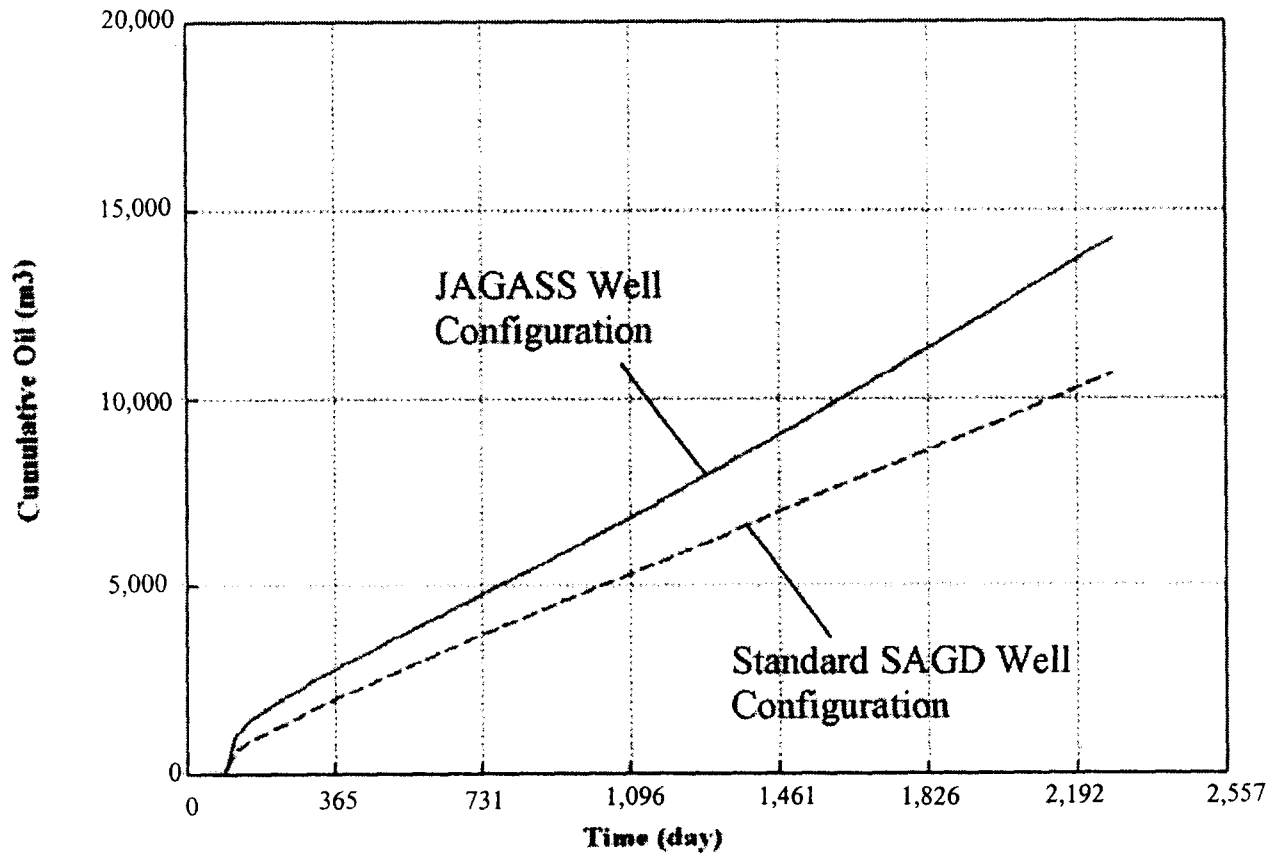


Figure 5

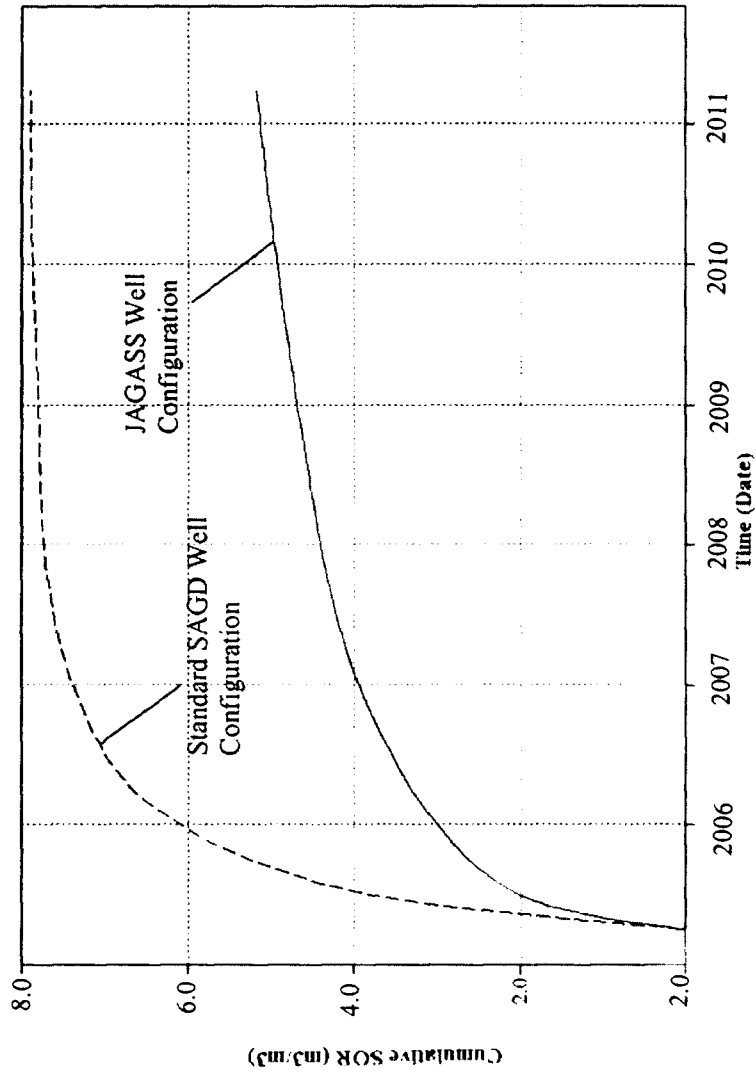


Figure 6a

$P = 1000 \text{ kPa}$ ,  $h = 8 \text{ m}$ ,  $kv = kh/5$

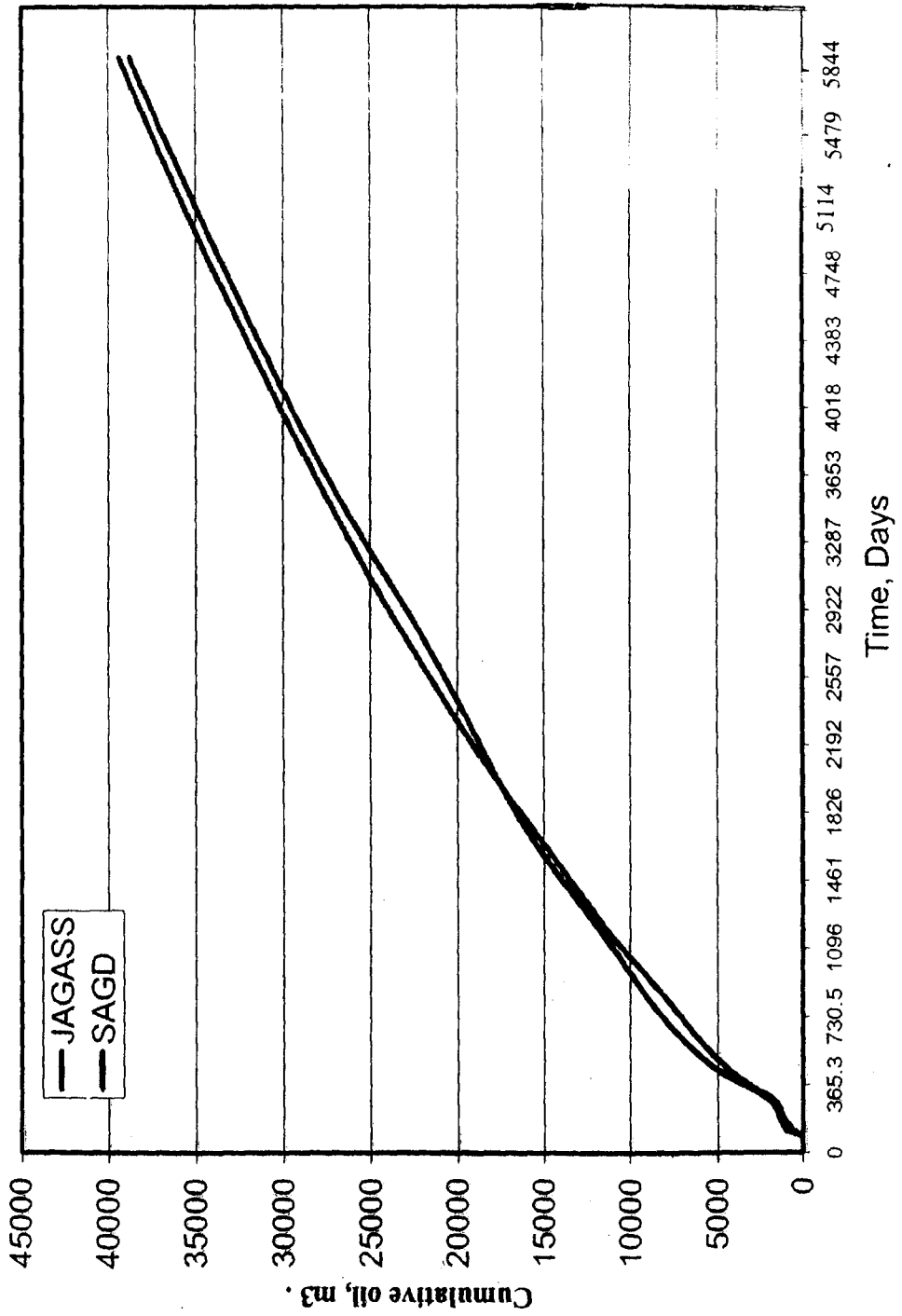


Figure 6b

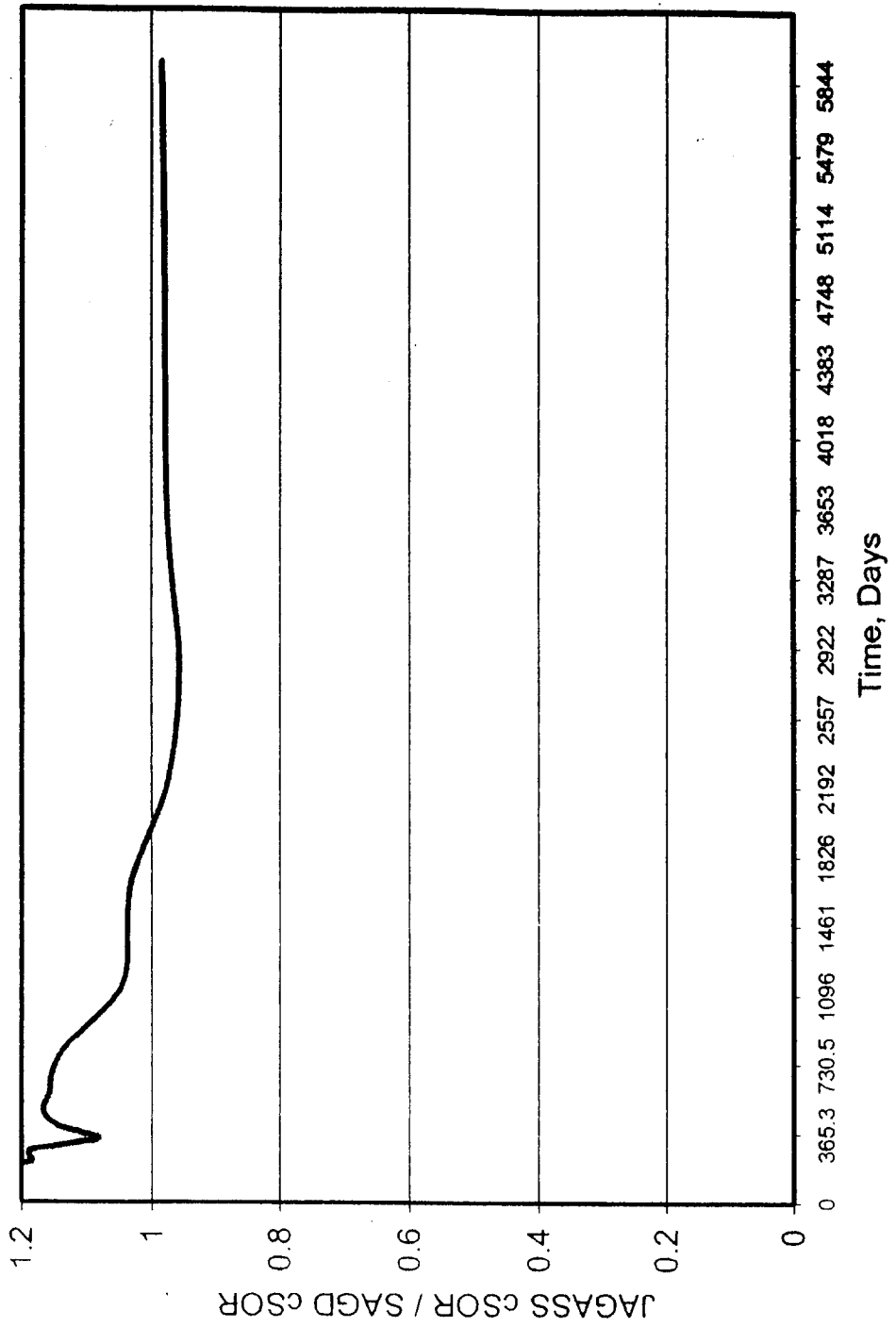


Figure 6c

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$P = 1000 \text{ kPa}, h = 15 \text{ m}, kv = kh/5$

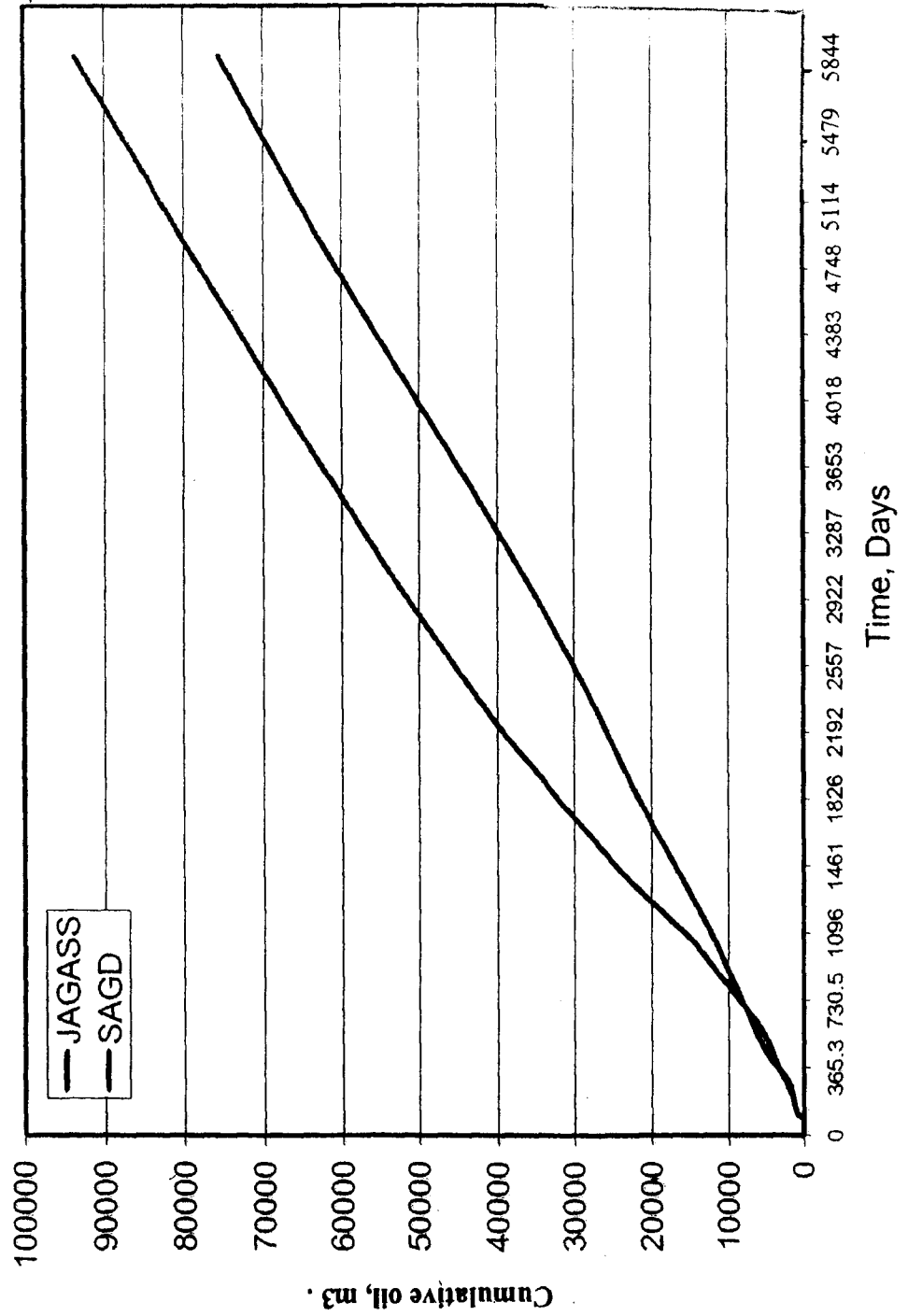


Figure 6d



**INTERNATIONAL SEARCH REPORT**

International application No.  
PCT/CA2007/001216

A. CLASSIFICATION OF SUBJECT MATTER  
**IPC: E21B 43/24 (2006.01)**  
 According to International Patent Classification (IPC) or to both national classification and IPC

**B. FIELDS SEARCHED**

Minimum documentation searched (classification system followed by classification symbols)  
 IPC (2006.01): E21B 43/16, 43/20, 43/24, 43/30  
 USPC: 166/268, 272.1, 272.3, 272.6, 272.7, 275

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic database(s) consulted during the international search (name of database(s) and, where practicable, search terms used)  
 Questel Orbit QWeb Pluspat, Delphion; keywords: SAGD, steam assisted gravity drainage, horizontal, well, inclined, heel, toe, inject+, produc+

**C. DOCUMENTS CONSIDERED TO BE RELEVANT**

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 5318124 A (ONG, T. S. et al.) 7 June 1994 (07-06-1994) *col. 2, l. 23-col. 3, l. 31; abstract, figures*	1-54
A	US 6167966 B1 (AYASSE, C. et al.) 2 January 2001 (02-01-2001) *whole document*	1-54
A	US 4248302 A (CHURCHMAN, R. K.) 3 February 1981 (03-02-1981) *whole document*	1-54
A	US 5016709 A (COMBE, J. et al.) 21 May 1991 (21-05-1991) *whole document*	1-54

Further documents are listed in the continuation of Box C.       See patent family annex.

* Special categories of cited documents :	"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"A" document defining the general state of the art which is not considered to be of particular relevance	"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"E" earlier application or patent but published on or after the international filing date	"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art
"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)	"&" document member of the same patent family
"O" document referring to an oral disclosure, use, exhibition or other means	
"P" document published prior to the international filing date but later than the priority date claimed	

Date of the actual completion of the international search 13 September 2007 (13-09-2007)	Date of mailing of the international search report 26 October 2007 (26-10-2007)
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Name and mailing address of the ISA/CA Canadian Intellectual Property Office Place du Portage I, C114 - 1st Floor, Box PCT 50 Victoria Street Gatineau, Quebec K1A 0C9 Facsimile No.: 001-819-953-2476	Authorized officer <b>Christian Opris 819- 934-4264</b>
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**INTERNATIONAL SEARCH REPORT**  
Information on patent family members

International application No.  
**PCT/CA2007/001216**

Patent Document Cited in Search Report	Publication Date	Patent Family Member(s)	Publication Date
US 5318124 A	07-06-1994	CA 2055549 A1 DE 4238247 A1 RU 2098613 C1	15-05-1993 19-05-1993 10-12-1997
US 6167966 B1	02-01-2001	NONE	
US 4248302 A	03-02-1981	CA 1122519 A1	27-04-1982
US 5016709 A	21-05-1991	CA 1332147 C FR 2632350 A1	27-09-1994 08-12-1989